

# Reinhold Environmental Ltd.

---



2009 NO<sub>x</sub>-Combustion Round  
Table & Expo Presentation

---

February 9 & 10, 2009, Cleveland, OH

# **Integrating In-Furnace Measurements with Combustion Optimization**

**Peter Spinney, Director of Market & Technology Assessment, NeuCo, Inc.**

**February 9, 2009**

**Reinhold Environmental NOx Roundtable**

# Outline

- CPS Energy J.T. Deely Power Plant
- CombustionOpt<sup>®</sup> Overview
- ZoloBOSS<sup>™</sup> System
- Integration of Combustion Optimization with Spectroscopy Sensors at J.T. Deely
- Initial Findings
- Next Steps

# CPS J.T. Deely Power Plant

- Owned and operated by CPS Energy
  - CPS 2nd largest municipally owned utility in the country
- J.T. Deely plant commissioned in 1977
- Two 446 MW Alstom-CE t-fired units w/Honeywell DCS
  - Unit 1 first in nation to integrate combustion optimization software with boiler optimization spectroscopy sensors

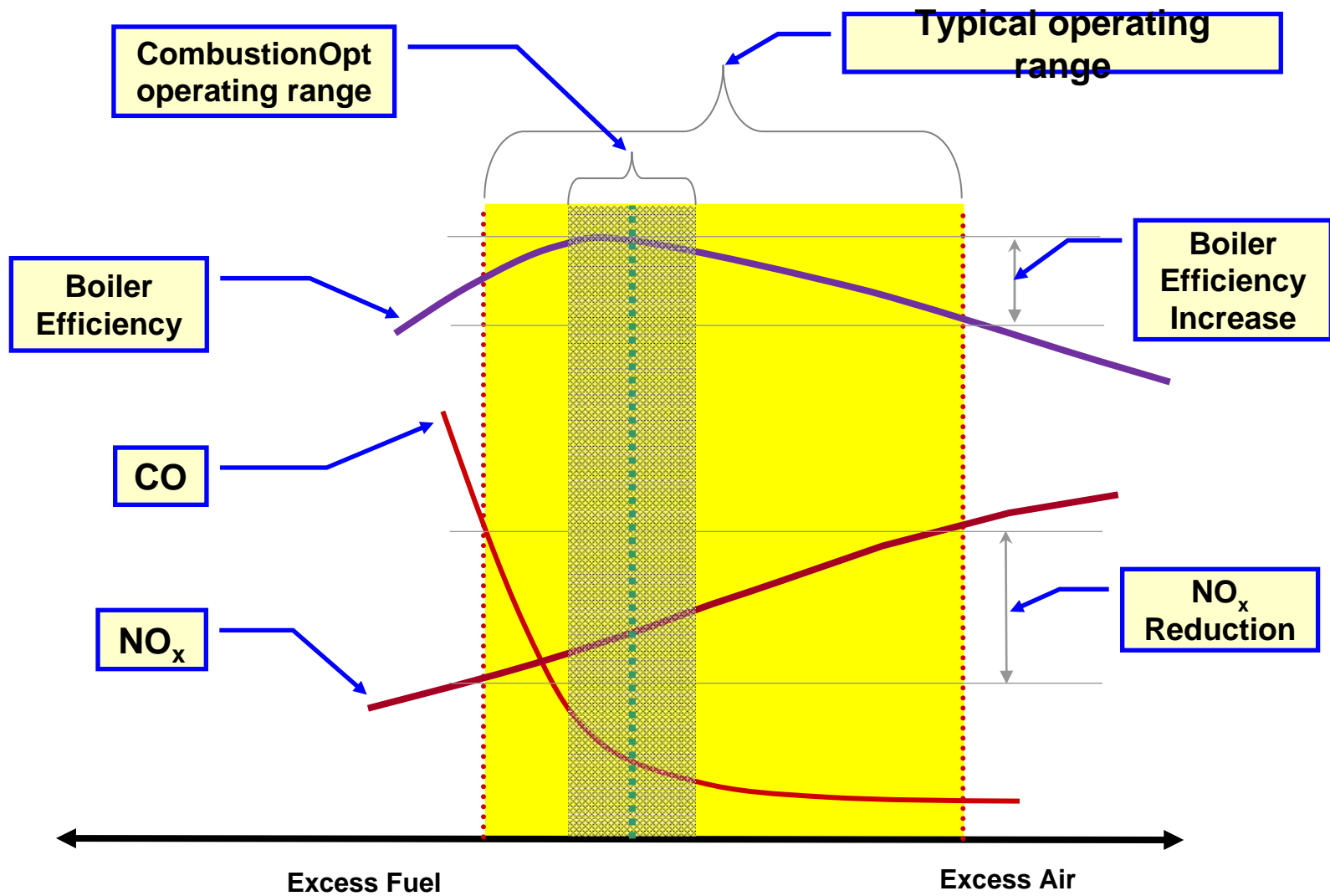
# CPS J.T. Deely Power Plant

- 1998 CPS committed to voluntarily reduce NOx emissions by 15 to 20%
  - Smaller SCRs when needed
  - Lower associated capital and O&M costs.
- TCEQ and State Senate enacted NOx rules in 2000
- J.T. Deely success with in-furnace NOx reduction
- Combustion optimization installed on both units in 2004
- Multivariate predictive control (MPC) added in 2007
  - Explicit steam temperature control
  - Minimize attemperation sprays
  - Incremental heat rate and NOx reduction

# CombustionOpt

- Provides real-time optimization & advanced control
- Utilizes 3 types of models:
  - Model-predictive control (MPC)
  - Neural networks with online learning
  - Engineering calculations
- Key goals for Deely
  - Minimize NO<sub>x</sub> (or control to a setpoint, depending on the season)
  - Maintain steam temperatures (average & side/side split)
  - Minimize sprays to reduce Heat Rate
  - Avoid plant constraints (high CO, damper positions, mill limits, etc.)

# CombustionOpt Optimization



## CombustionOpt Home

10/9/2008 12:33 PM (1 day)

### Optimization Alerts

Issue	Actual	Target	!!!	NOx Svngs (...)	Fuel Svngs (...)	Relative Impa...
C'Opt MVs disabled Trigger (U...	70.37	100	!!!!	12,896	39,206	<div style="width: 100%; height: 10px; background-color: red;"></div>

### Optimization Benchmarks

Benefits (month)					
Objectives	Units	Achieved (vs. Baseline)		Achievable (vs. Actual)	
Fuel	Btu/KWh	176.06	<div style="width: 100%; height: 10px; background-color: green;"></div>	41.98	<div style="width: 100%; height: 10px; background-color: green;"></div>
Fuel	\$	98,900.52	<div style="width: 100%; height: 10px; background-color: green;"></div>	29,478.2	<div style="width: 100%; height: 10px; background-color: green;"></div>
NOx	lb/MBtu	0.01	<div style="width: 100%; height: 10px; background-color: green;"></div>	0.01	<div style="width: 100%; height: 10px; background-color: green;"></div>
NOx	\$	24,542.81	<div style="width: 100%; height: 10px; background-color: green;"></div>	12,541.85	<div style="width: 100%; height: 10px; background-color: green;"></div>

### Optimization Analysis

Supervisory Profile: 10/9/2008 12:30:46 PM

[Analysis...](#)

MV Name	Pre-Move	Post-Move	Delta Move	Objectives	Actual	Predicted	Target	Delta Cost
AUXDPR AA SEL	-0.928	-0.944		NOx (lb/MBtu)	0.0930	0.0929	Down	
AUXDPR AB SEL	4.955	4.969		IDF 3A Amps	444.3	442.0	< 445 (A)	
AUXDPR BC SEL	-10	-10		IDF 3B Amps	457.5	457.2	< 445 (A)	
AUXDPR CD SEL	-0.13	-0.161		Sum of Fdr Bi	-0.09	-0.07	0	
AUXDPR DE SEL	-6.559	-6.528		IDF 3C Amps	432.3	426.5	< 445 (A)	
AUXDPR EF SEL	2.663	2.665		Mill 3C dP (in)	7.56	7.56	< 7.5 (inH)	
AUXDPR FF SEL	10	10		Mill 3A dP (in)	7.42	7.42	< 7.5 (inH)	
FEEDER A SEL BI	-6.841	-6.856		Mill 3F dP (in)	7.19	7.18	< 7.5 (inH)	
FEEDER B SEL BI	5	5		Opacity (perc)	18.82	18.61	< 23 (perc)	
FEEDER C SEL BI	-1.6	-1.631		RH Spray Flo	5.77	-0.87	< 25 (klb/h)	
FEEDER D SEL BI	5	5		O2 3 & 4 (perc)	3.39	3.39	> 2.5 (perc)	
FEEDER E SEL BI	-0.203	-0.078		Mill 3B dP (in)	5.87	5.87	< 7.5 (inH)	
FEEDER F SEL BI	-1.442	-1.507		Mill 3D dP (in)	7.95	7.95	< 7.5 (inH)	
FUEL AIR A SEL	5	5		O2 1 & 2 (perc)	3.04	3.04	> 2.5 (perc)	
FUEL AIR B SEL	-5	-5		Sum of Aux B	0.00	0.00	0	
FUEL AIR C SEL	-5	-5		Mill 3E dP (in)	6.56	6.57	< 7.5 (inH)	
FUEL AIR D SEL	-5	-5		O2 Split (perc)	-0.35	-0.37	0	
FUEL AIR E SEL	-1.392	-2.815		Heat Rate (Bt	10312.3	10322.6	Down	
FUEL AIR F SEL	-3.692	-2.51						
G SOFA TILT SEL	0	MV Disabl						
GA SOFA DMPR	0	MV Disabl						

### Setpoints (Deviations)

Setpoint	Units	Actual	Target
O2 Split	percent	-0.22	-0.08
Sum of Fdr Bia	unitless	7.51	0.61
Sum of Aux Bk	unitless	-0.01	0

### Limits (%Violations)

Limit	Units	Actual	Target
Opacity	percent	0	0
O2 1, 2	percent	-12.95	14.44
O2 3, 4	percent	0	0
RH SF	klb/h	-6.57	-2.26
Mill 3A	inH2O	7.2	-0.54
Mill 3R	inH2O	0	0

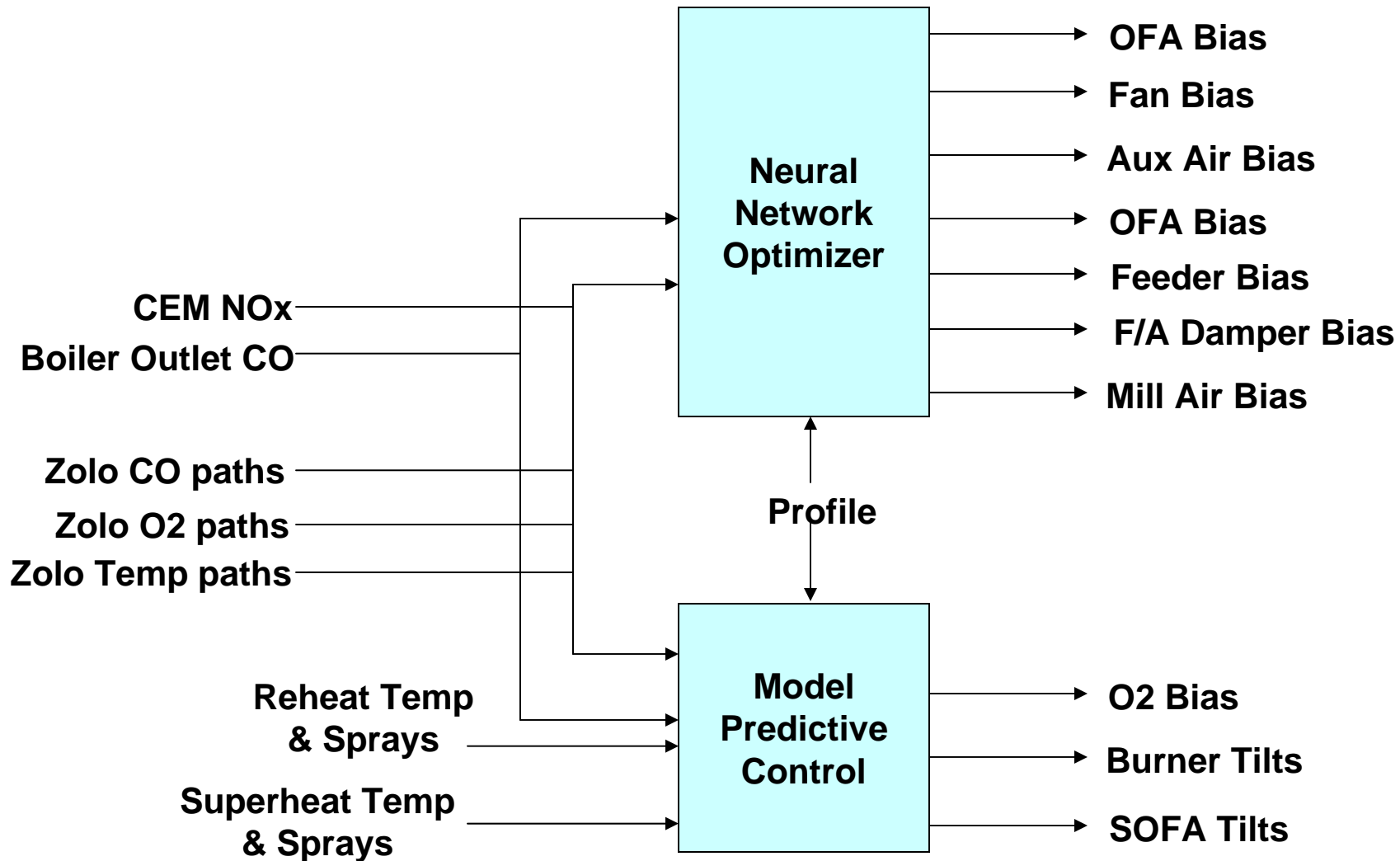
# ZoloBOSS System

- Measures and maps multiple constituents directly in the furnace
- Tunable diode laser absorption spectroscopy
- Scans a laser in wavelength across the known absorption for a given constituent (i.e. CO)
  - Compares the amount of light absorbed by the constituent with the amount of light that traversed the boiler
- Up to 10,000 measurements per second
  - Each measurement has its own calibration for dust, ash, turbulence, and drift

# CombustionOpt with ZoloBOSS at Deely

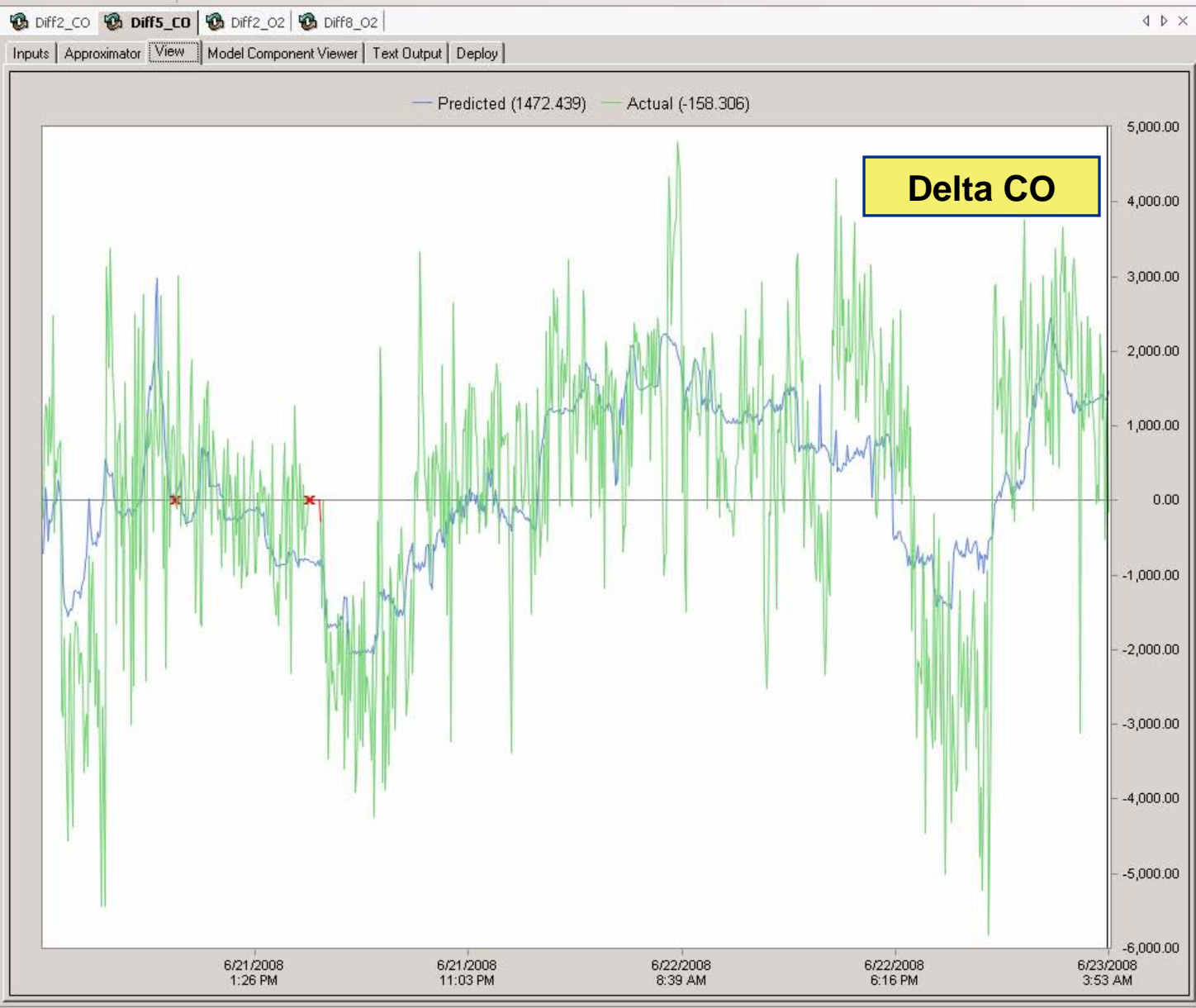
- CombustionOpt successfully used for several years
- Deely was the first site where MPC was integrated with neural, providing additional benefits
- Deely realizing between 0.12 and 0.13 lbs/mmbtu but had set a goal of 0.08 lb/mmbtu
- Motivations for adding ZoloBOSS
  - New unit at Spruce created additional NOx pressure
  - Increasing coal costs
  - Innovative culture and commitment to continuous improvement
  - Recognition that higher resolution measurements of key combustion indicators could provide additional performance gains

# CombustionOpt w/ZoloBOSS at Deely 1





- Enterprise
  - Collections
  - Data Documents
  - Deely U1 Problem
  - Forms
  - New TriggerConc
  - Tasks
  - Roles
  - U1 Data & Services 1020
  - PipelineFunctions
  - Project Version
  - Sources
  - Variable Sets
  - Variable Trees
  - Sensors
  - Servers & Services
  - Tools
  - Models
    - Diff CO
      - Diff1\_CO
      - Diff2\_CO
      - Diff3\_CO
      - Diff4\_CO
      - Diff5\_CO
      - Diff6\_CO
      - Diff7\_CO
      - Diff8\_CO
      - Diff9\_CO
    - Diff\_O2
      - Diff1\_O2
      - Diff2\_O2
      - Diff3\_O2
      - Diff4\_O2
      - Diff5\_O2
      - Diff6\_O2
      - Diff7\_O2
      - Diff8\_O2
      - Diff9\_O2
  - Roles
  - Retune Profiles
  - U1 Diagnostic Utilities V2:
  - U1 Diagnostics Utilities 10
  - U1 Trending and Analysis
- Users
- System of Units
- Services
- Task Queues
- Enterprise

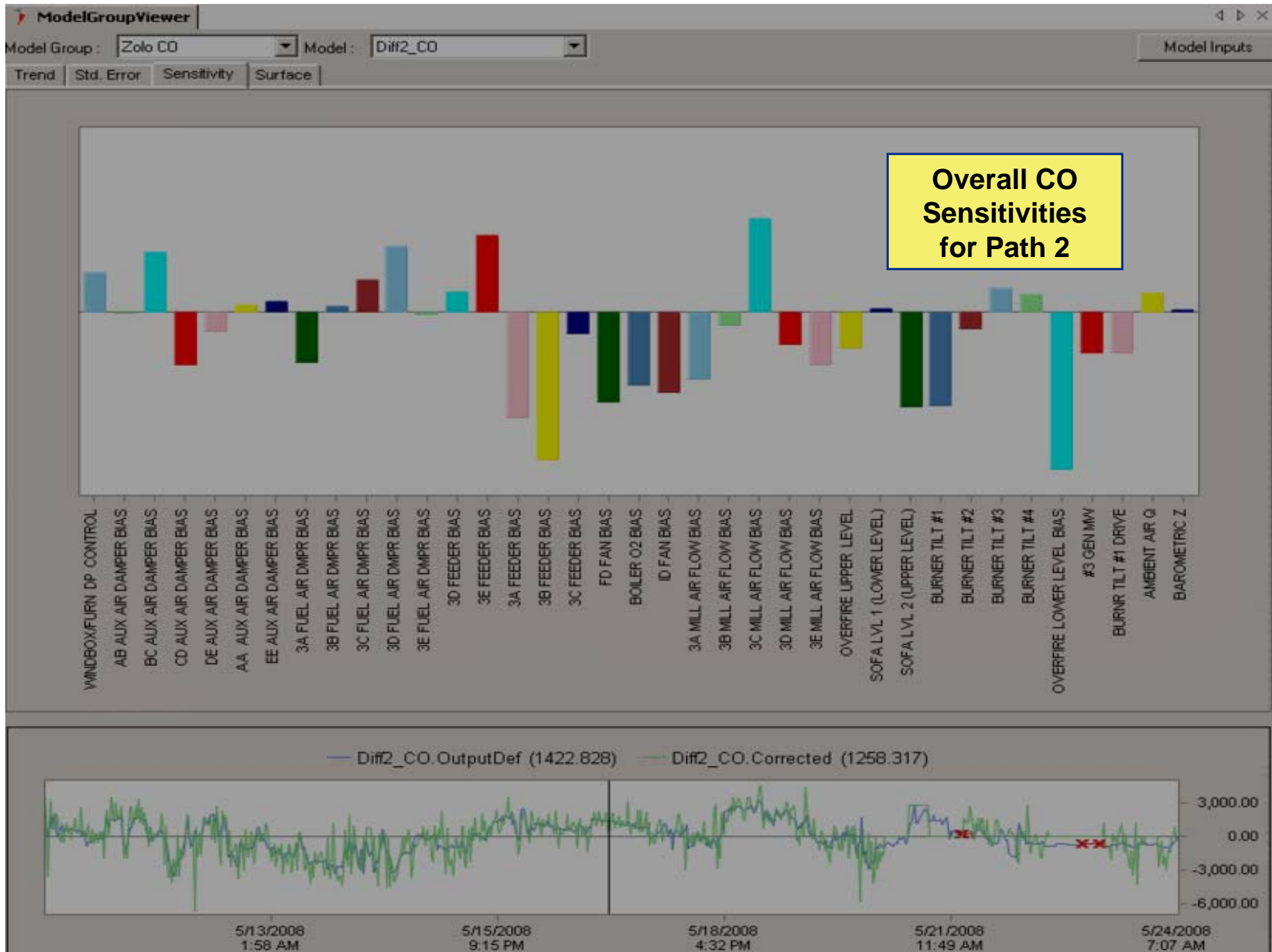


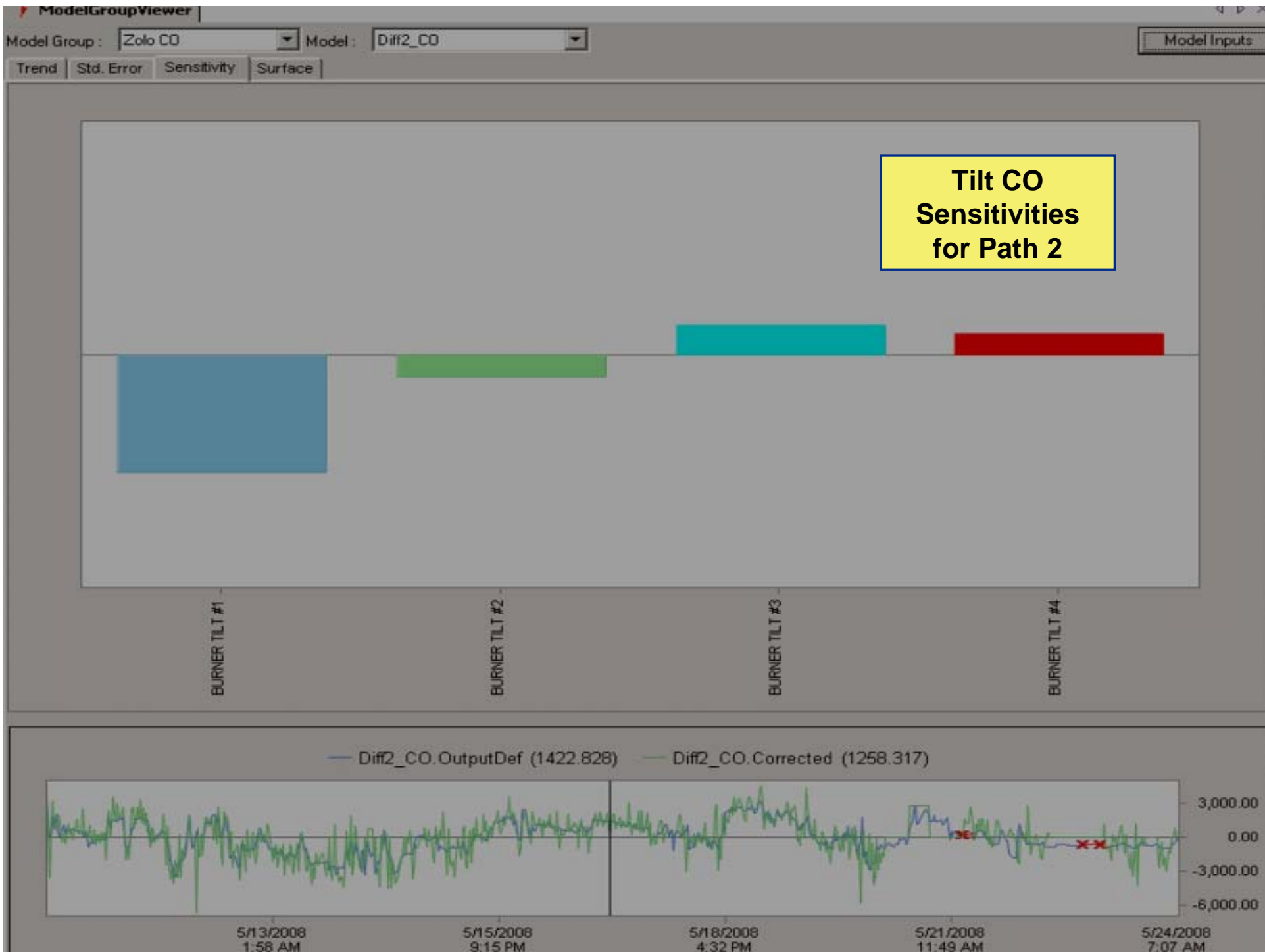
Diff7\_CO (Modelle... x

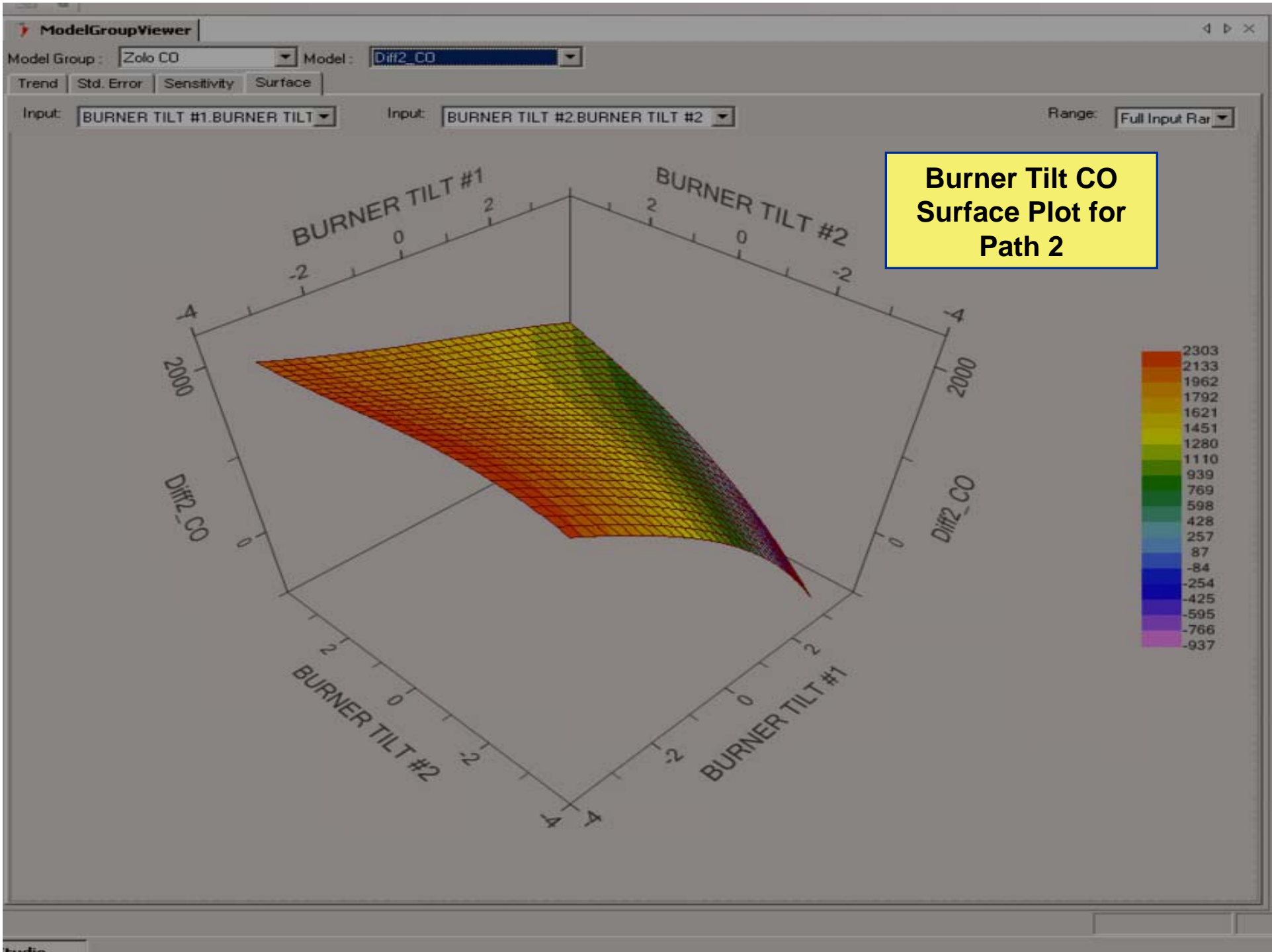
Name	Value
InitialPrior...	0
Created	4/17/2008
Modified	6/19/2008

Diff7\_CO (Modelle... x

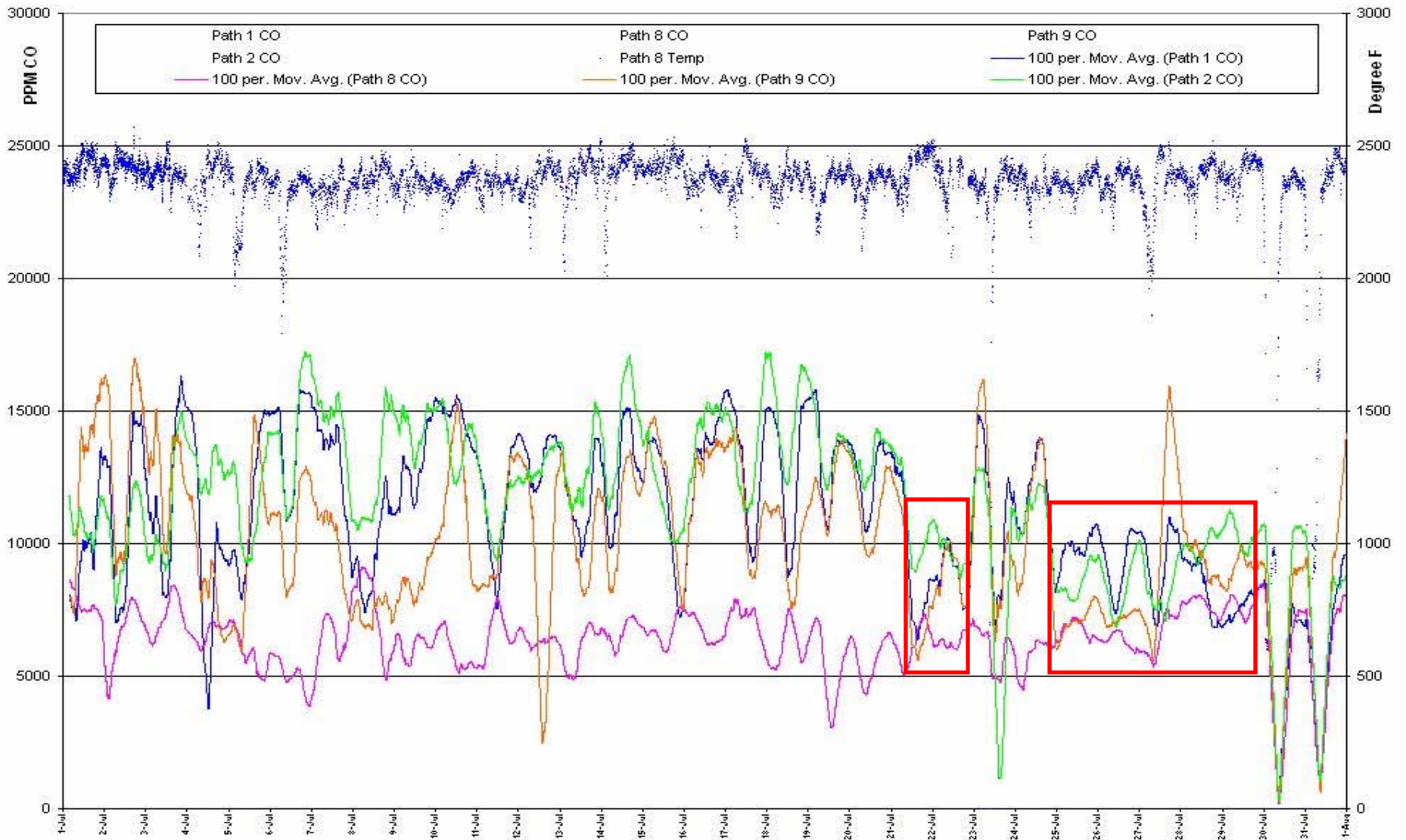
- Name
- Inputs
- Expected
- Outputs
- Statistics
- Sensitivity





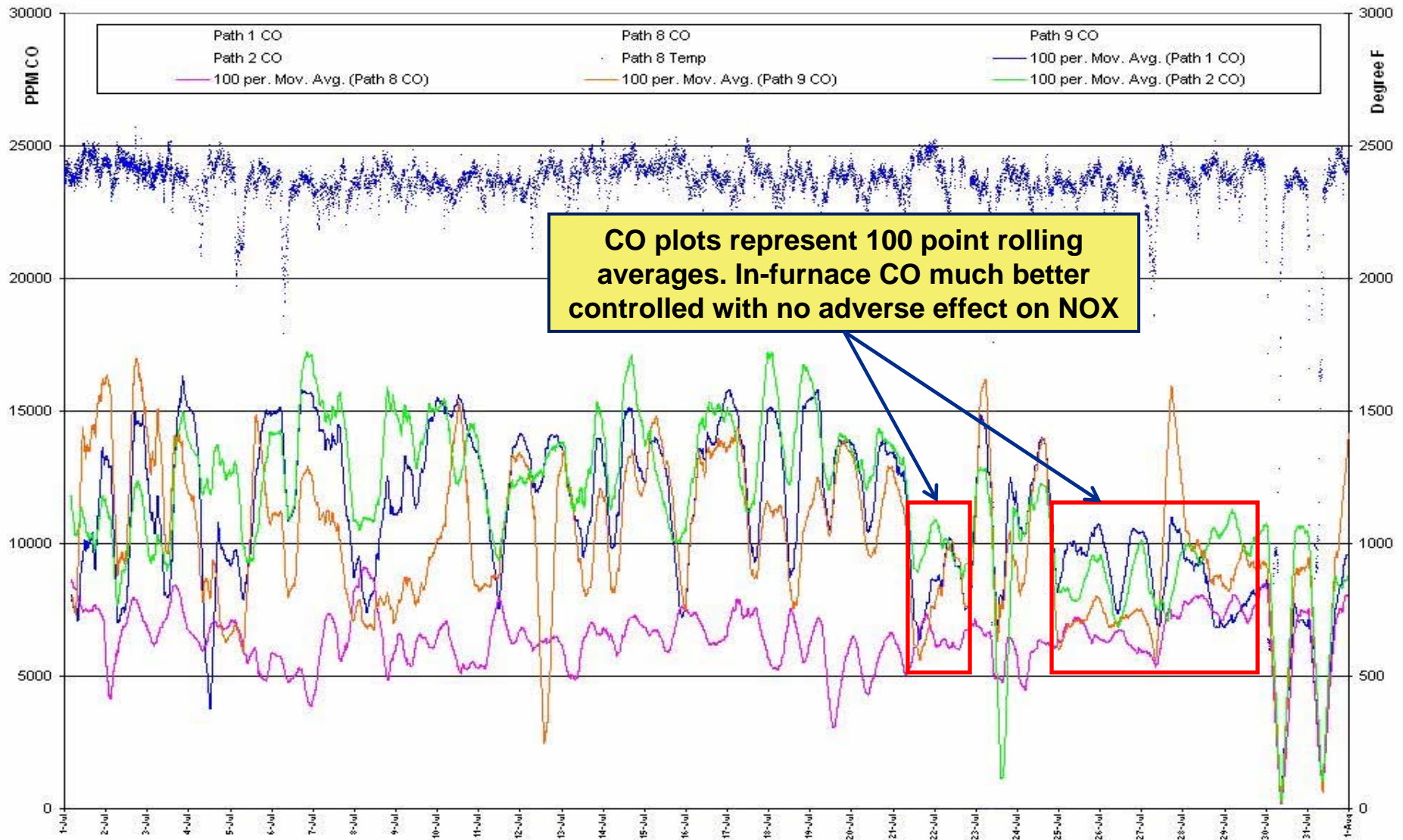


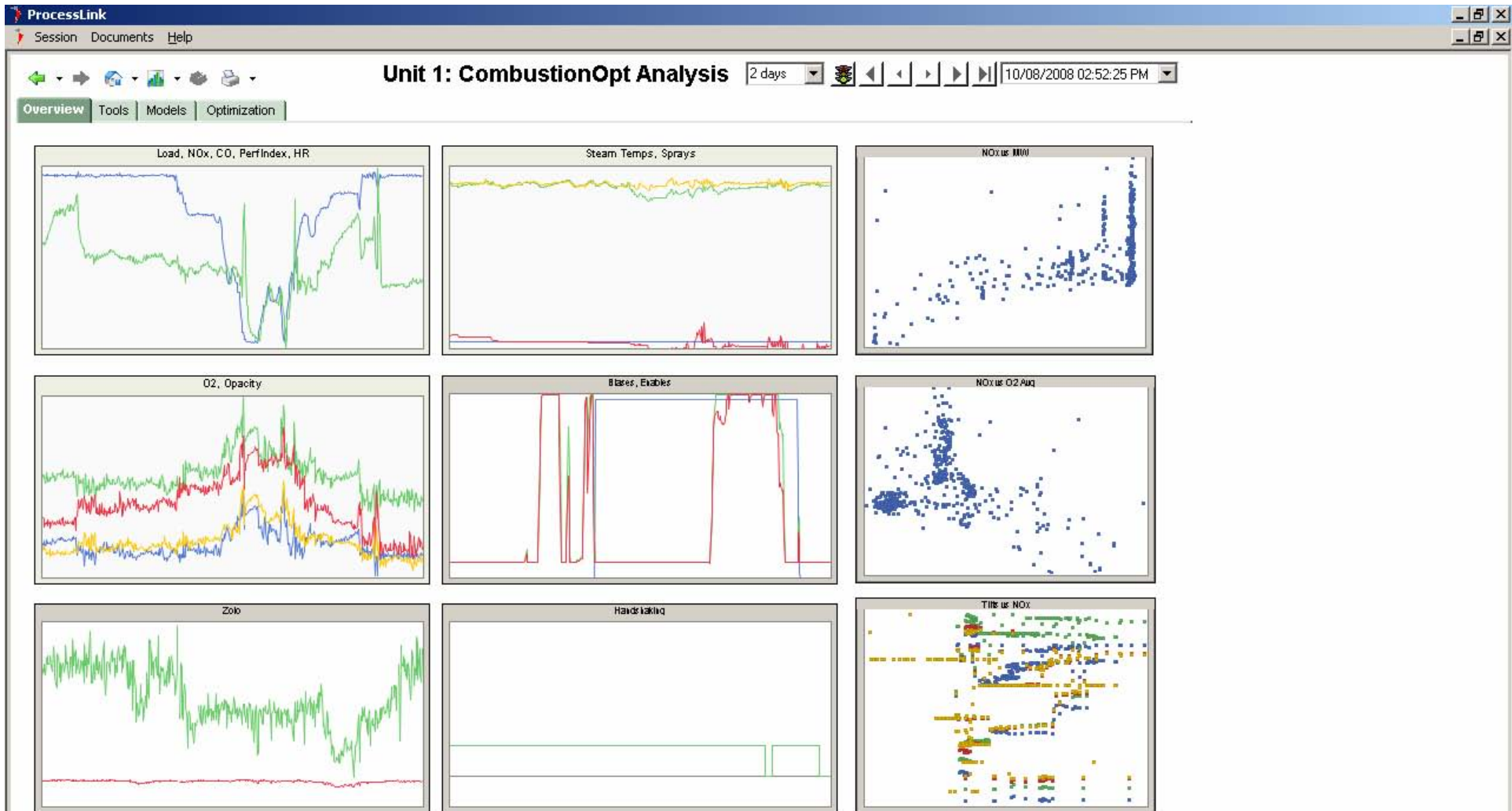
### JT DEELY, JULY '08



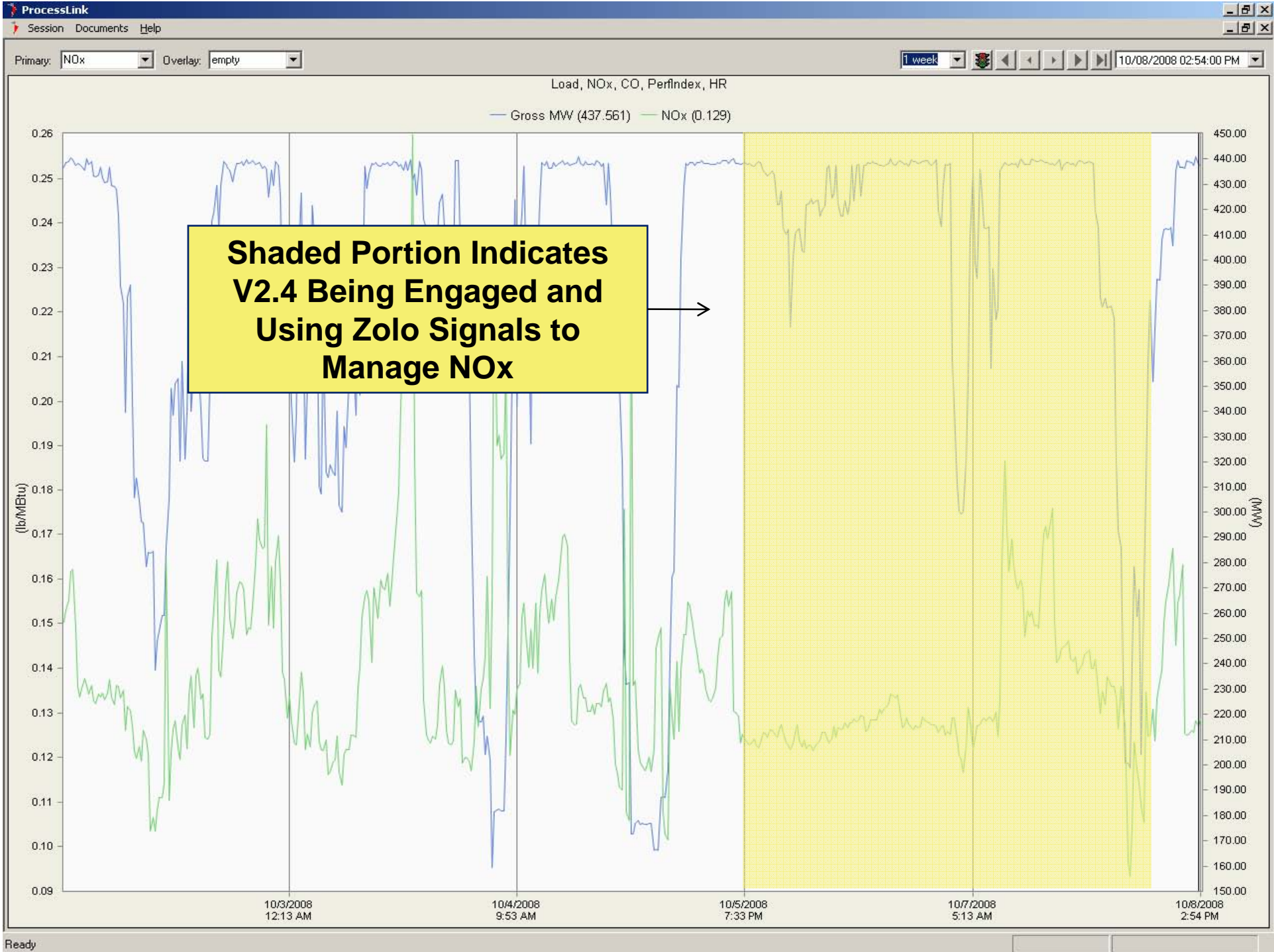
# Initial Experiments Controlling Zolo In-Furnace CO

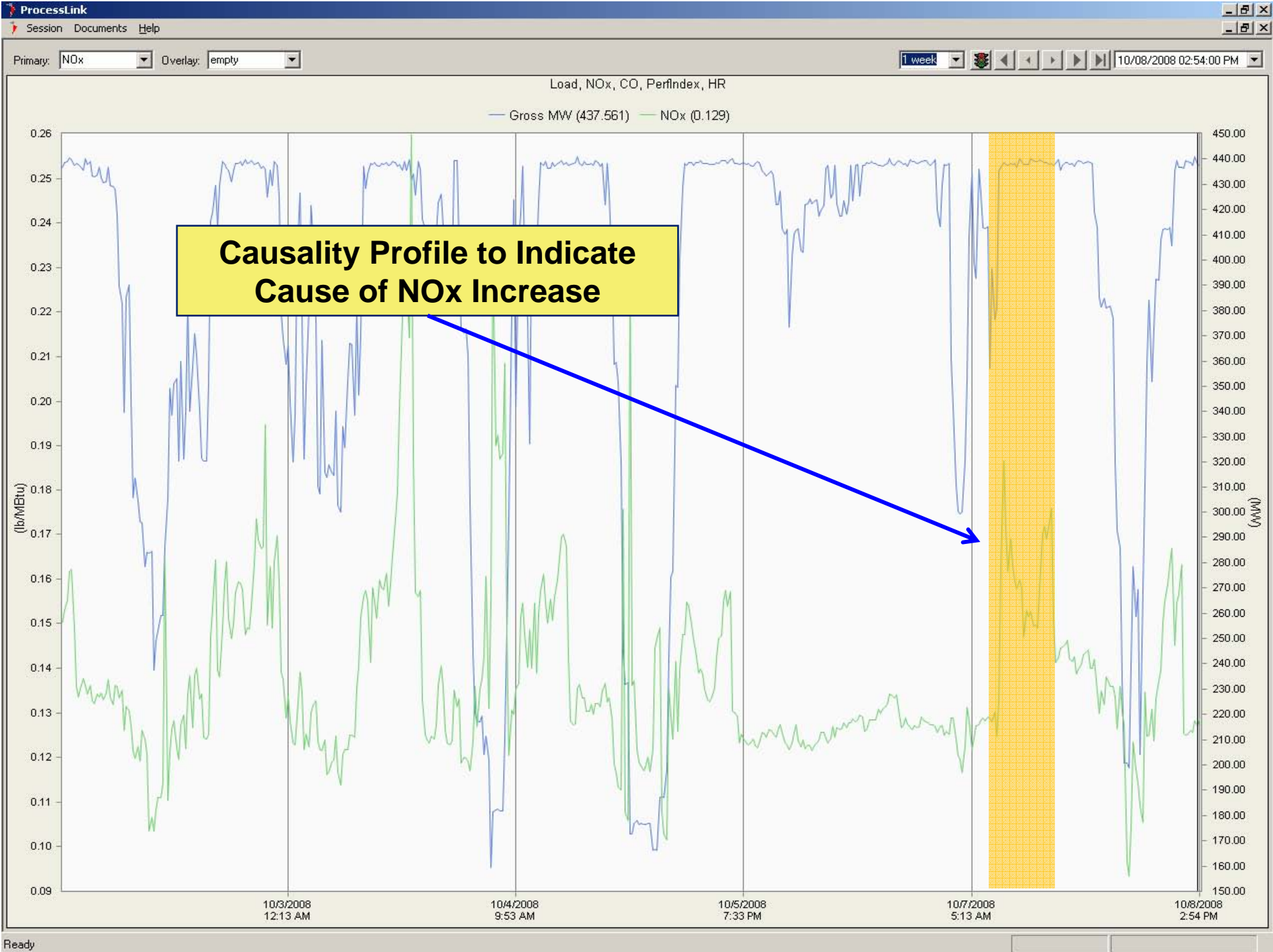
JT DEELY, JULY '08

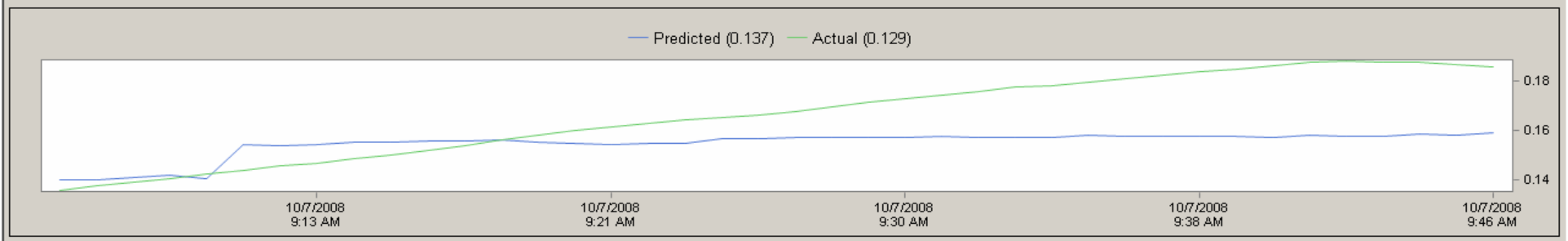
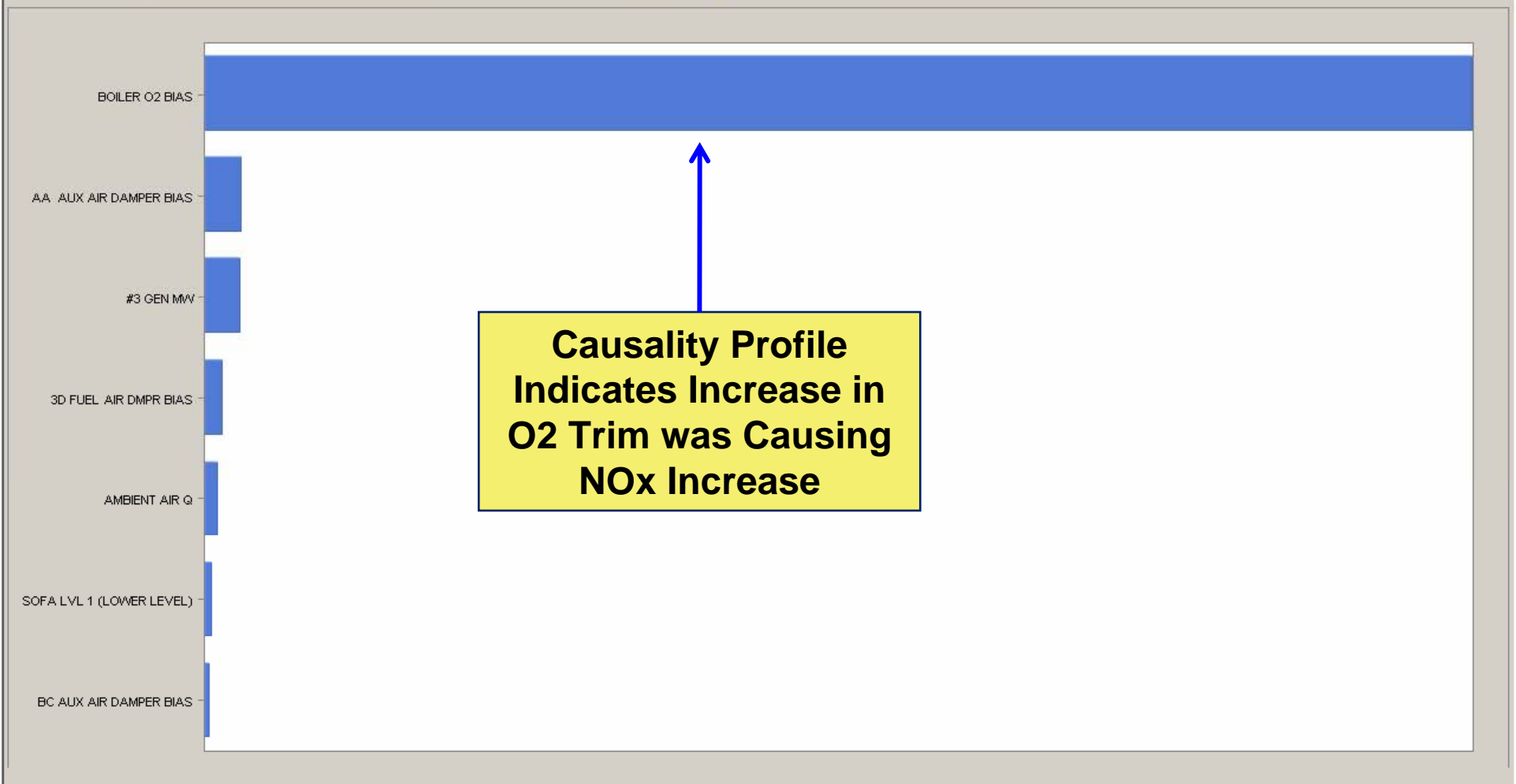


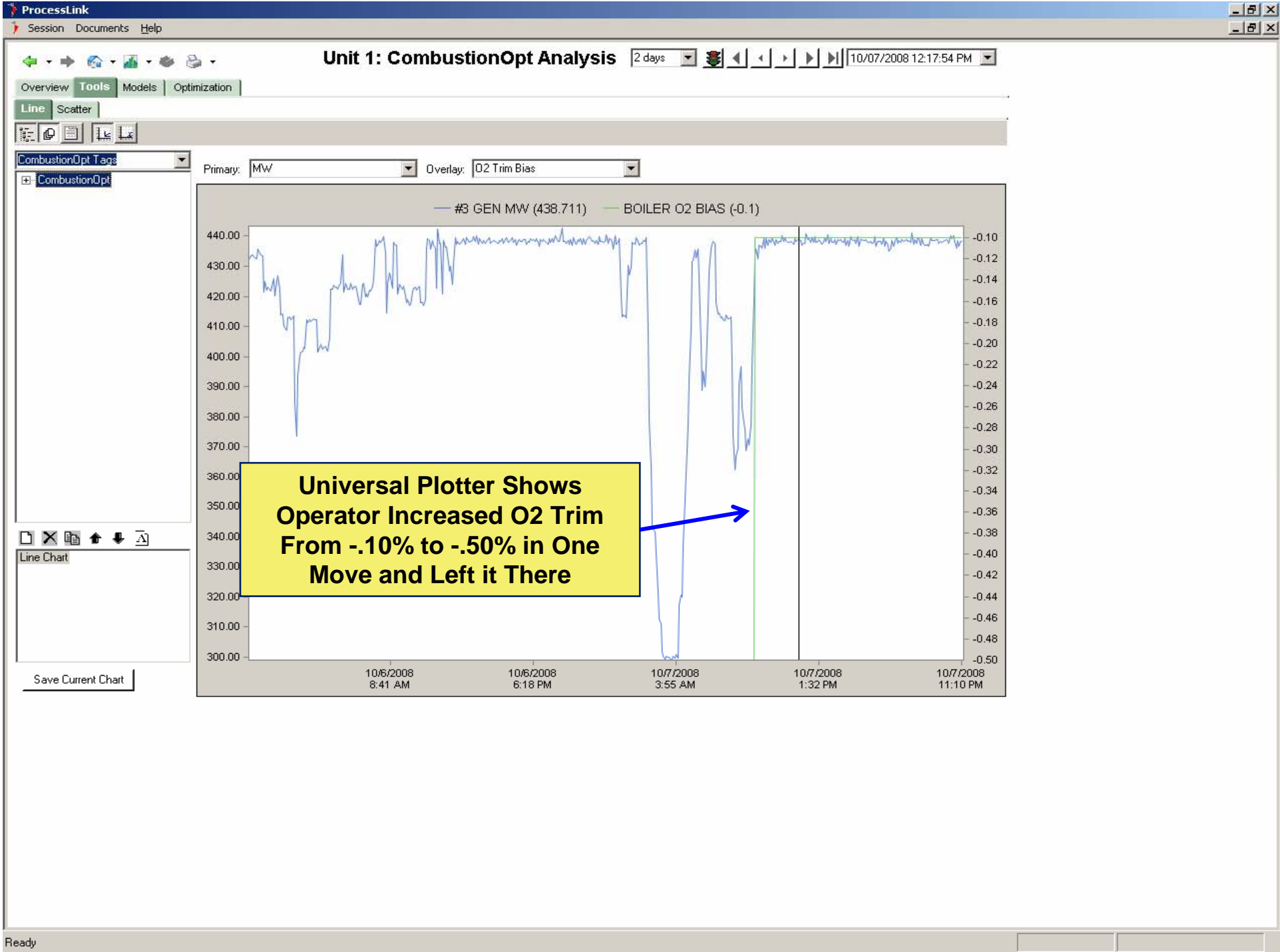


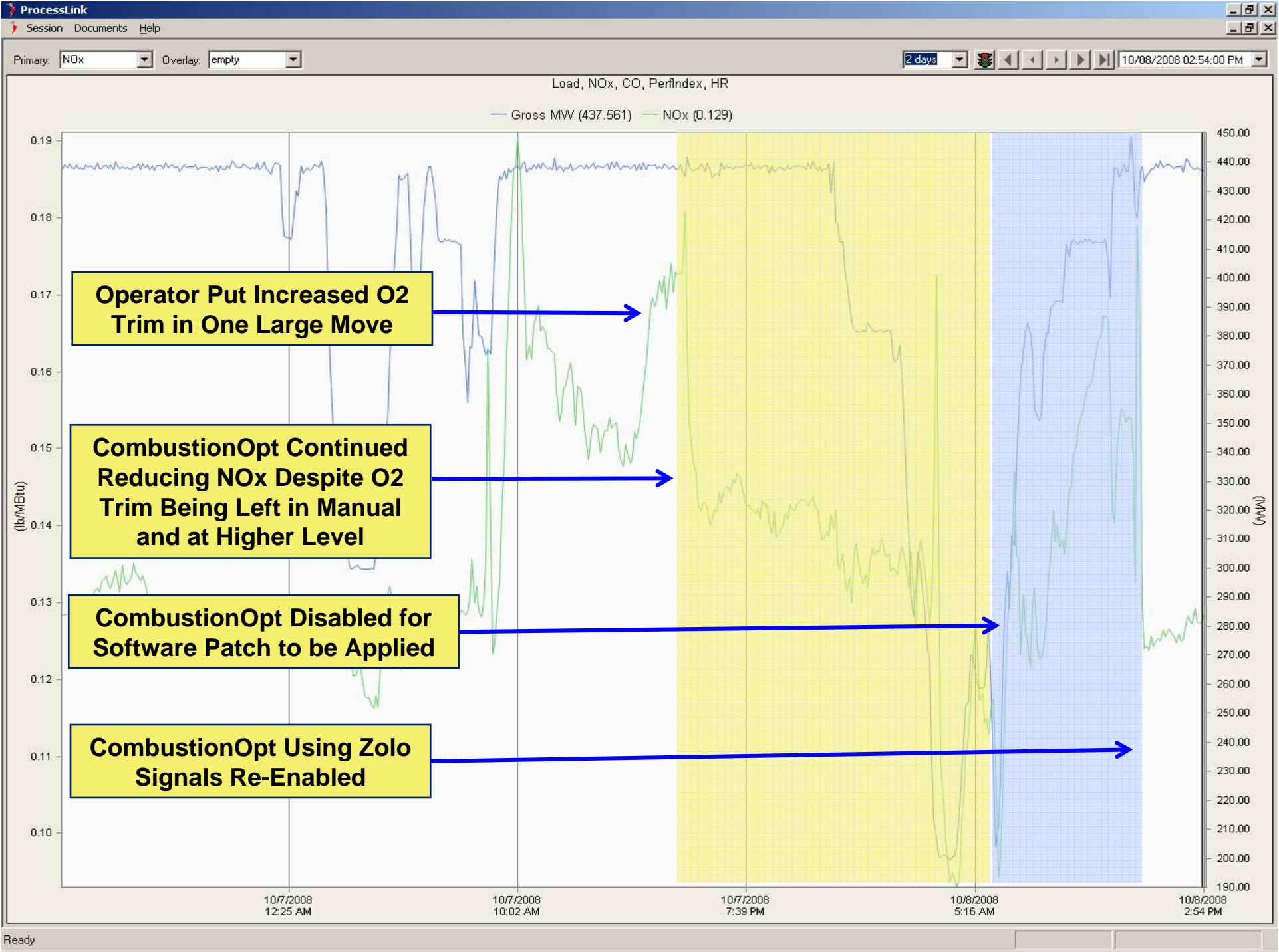
**CombustionOpt Analysis Screen Shows Overall Unit Operating Parameters Over Selected Span (2 Days)**











ProcessLink  
Session Documents Help

Unit 1: CombustionOpt Home 10/8/2008 03:13 PM (1 day)

### Optimization Alerts

Issue	Actual	Target	Fuel Svngs (...)	NOx Svngs (...)	Relative Imp...
PL Master is disabled Trigger	0	1	1,796	1,488	

### Optimization Benchmarks

Benefits (month)

Objectives	Units	Actual	Target
Boiler NOX	unitless	0	0
PerfIndex	unitless	3.58	0.03

### Optimization Analysis

MV Name	Pre-Move	Post-Move	Delta Move
WINDBOX/FURN	0	0.2	
AB AUX AIR DAM	-0.541	-1.147	
BC AUX AIR DAM	5	5	
CD AUX AIR DAM	4.105	5	
DE AUX AIR DAM	0	-0.554	
AA AUX AIR DAM	0.077	0.956	
EE AUX AIR DAM	0	1	
SOFA LVL 1 (LO	0	-1.5	
SOFA LVL 2 (UPP	0	-1.5	
BURNER TILT #1	0.222	0.122	
BURNER TILT #2	1.478	1.378	
BURNER TILT #3	-1.538	-1.638	
BURNER TILT #4	2.297	2.397	
3A FUEL AIR DM	-5	-5	
3B FUEL AIR DM	-5	-5	
3C FUEL AIR DM	1.482	2.194	
3D FUEL AIR DM	-5	-5	
3E FUEL AIR DM	-5	-5	
3D FEEDER BIAS	-2	-2	
3E FEEDER BIAS	-3.2	<i>MV Disabl</i>	
3A FEEDER BIAS	3.893	<i>MV Disabl</i>	

### NN C'Opt Closed Loop Profile: 10/8/2008 1:08:27 P Analysis...

Objectives	Actual	Predicted	Target	Delta Cost
Boiler NOX	0.127	0.125	Down	
Zolo Path 1 O	1.13	0.99	> -.5 and <	
Zolo Path 2 O	-0.75	-0.63	> -.5 and <	
Zolo Path 9 O	0.60	0.42	> -.5 and <	
Zolo Path 3 O	0.65	0.58	> -.5 and <	
Zolo Path 6 O	0.57	0.51	> -.5 and <	
Zolo Path 4 O	-0.25	-0.03	> -.5 and <	
Zolo Path 8 O	-0.75	-0.74	> -.5 and <	
Zolo Path 5 O	0.00	0.00	> -.5 and <	
PerfIndex	968.5	968.5	Down	
Sum of Feede	3.6	3.6	0	
Zolo Path 7 O	-0.07	-0.09	> -.5 and <	

### Setpoints (Deviations)

Sum of Feeder	unitless	0	0
---------------	----------	---	---

### Limits (%Violations)

Zolo Path 1 O2	unitless	20.96	31.9
Zolo Path 2 O2	unitless	12.9	36.52
Zolo Path 3 O2	unitless	39.46	-3.7
Zolo Path 4 O2	unitless	38.5	12.24
Zolo Path 5 O2	unitless	9.98	20.91

**CombustionOpt Home Page  
Indicating Optimizer is Using Zolo  
O2 Path Signals for Overall Goal  
of NOx Reduction**

# Initial Findings

- ZoloBOSS signals are consistent with manual testing and CPS observations
- CombustionOpt able to accurately model ZoloBOSS signals
  - Individual sensors
  - Deviations across paths
- High model quality, in terms of both correlation and normalized mean squared error
- CombustionOpt able to minimize CO and O2 deviations within furnace and use better spatial resolution to better control NOx
- Inadvertent “On vs. Off” test demonstrated benefits

# Next Steps

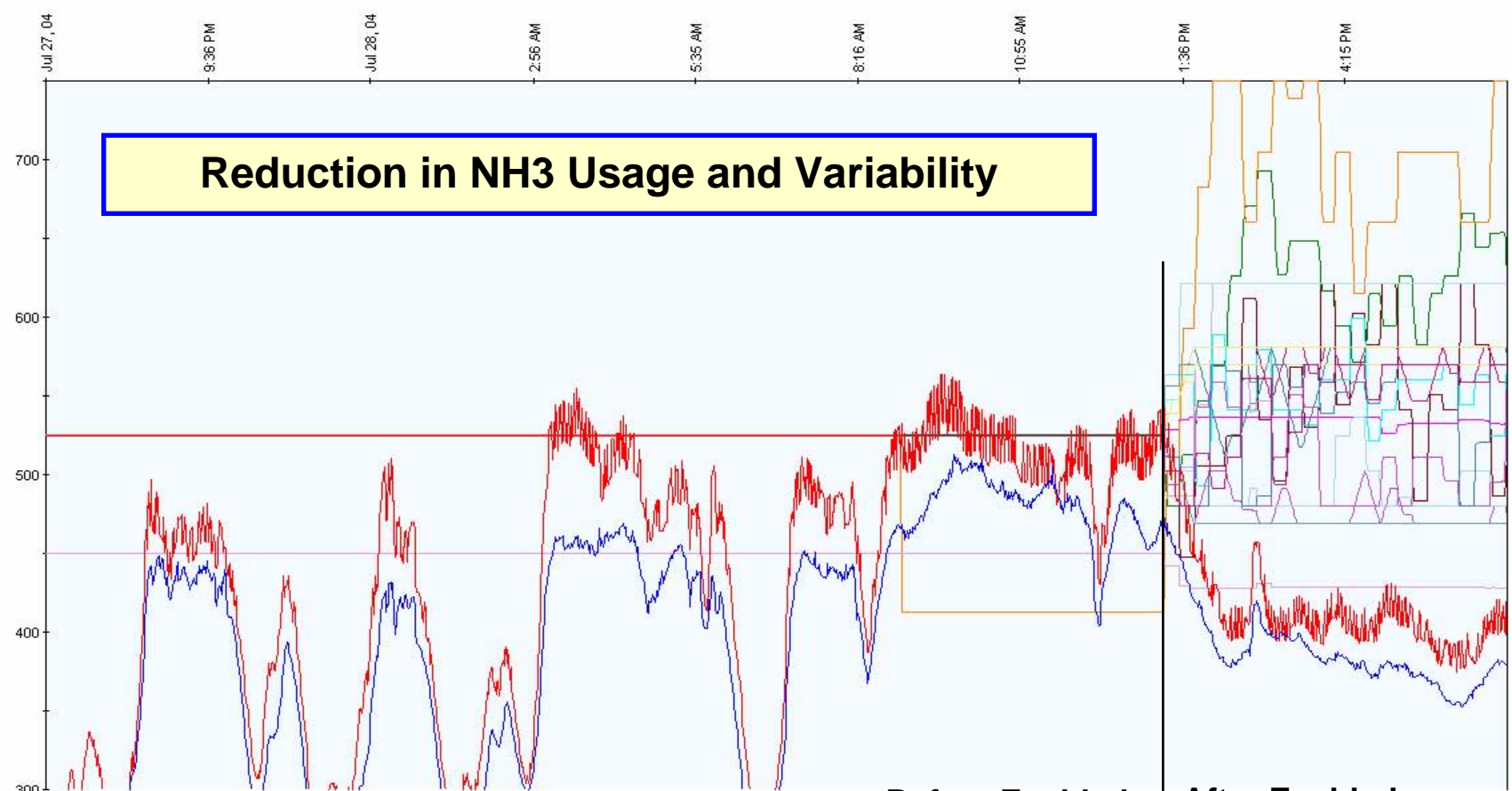
- Continue using Zolo models for optimization
- Employ validated models for optimization
  - Minimize deviation along and across paths
    - O<sub>2</sub>, CO, furnace temperatures
  - Minimum O<sub>2</sub> and/or maximum CO constraints
- Observe impacts of additional inputs and objectives on overall unit performance
  - Incremental NO<sub>x</sub> and heat rate reduction
  - Tradeoffs between local and global objectives/constraints
- Tune Optimization Profile based on testing and observation
- Quantify initial benefits
- Examine prospects for individual aux air damper biasing

# SCR/SNCR Systems & Optimization

- Reduce Reagent Usage
- Lengthen Maintenance Intervals
- Avoid Ammonia Slip
- Reduce risk of Ammonium Bisulfate & Sulfur Trioxide deposits
- Control “Blue-Plume” Excursions
- Better Manage Combustion  
Combustion

system



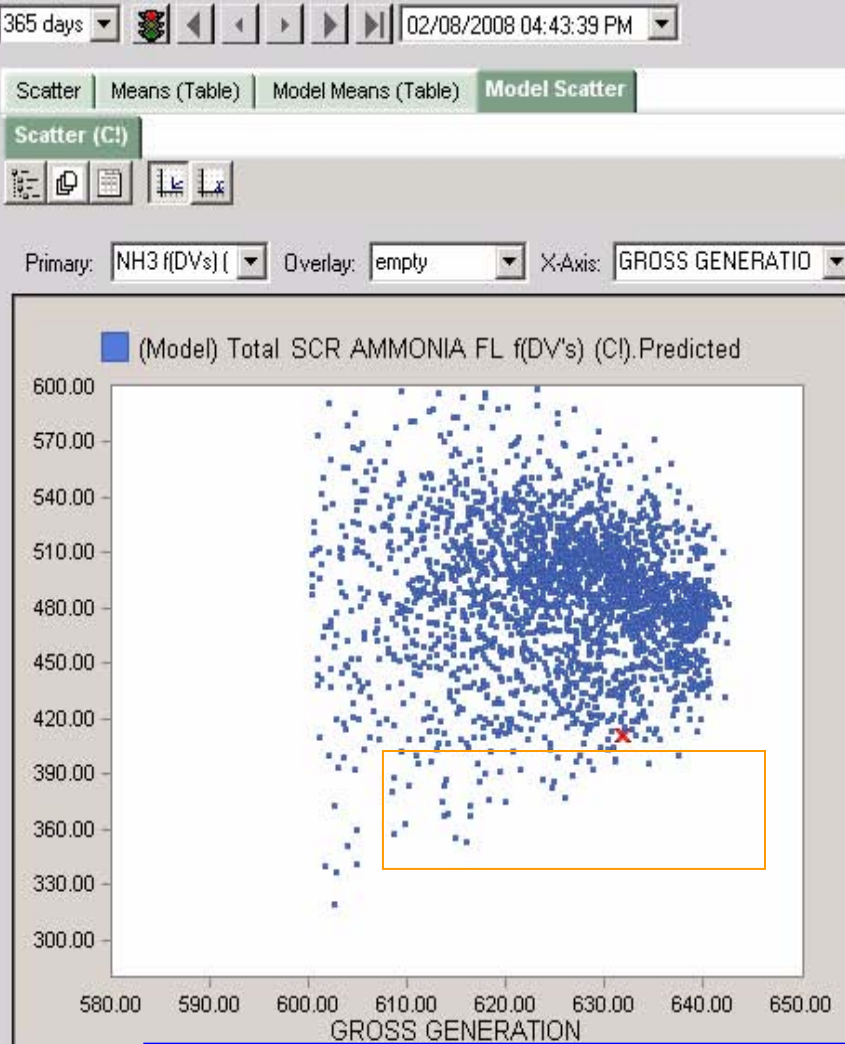


**Reduction in NH3 Usage and Variability**

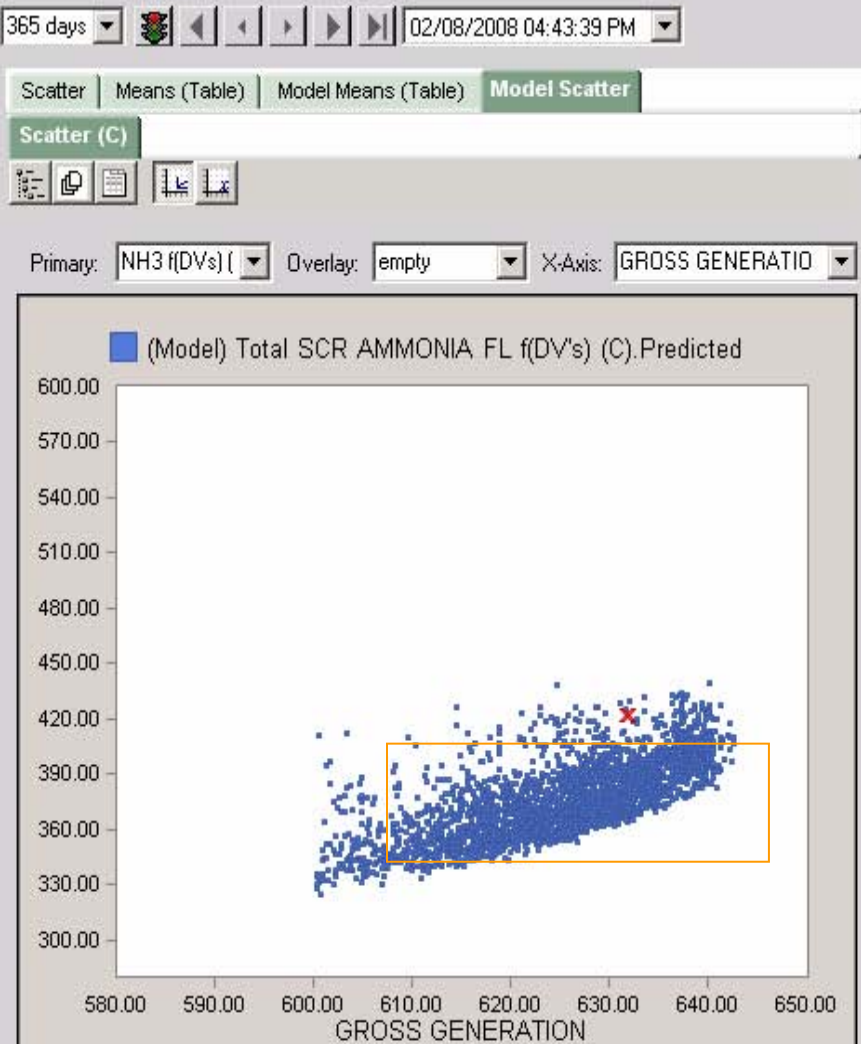
**Before Enabled**      **After Enabled**

- |  |   |  |   |
|--|---|--|---|
| — SCR 1A SELECTED AMMONIA FL (397.5097)  | — SCR 1B SELECTED AMMONIA FL (378.595)      | — U1 WBox/Furn DP Cntrl PL App (0.9104566) | — U1 Furn Press Cntrl PL App (0.0498)       |
| — 1 OFA Mstr Flow Cntrl PL App (50)      | — 1 OFA RFA Flow Cntrl PL App (-3)          | — 1 OFA LFB Flow Cntrl PL App (6)          | — 1 OFA RRC Flow Cntrl PL App (15)          |
| — 1 OFA LRD Flow Cntrl PL App (15)       | — ID Fan 1A Inlet Vlv Dmd PL App (-2.23289) | — ID Fan 1B Inlet Vlv Dmd PL App (2.27731) | — ID Fan 1C Inlet Vlv Dmd PL App (1.467699) |
| — U1 Air/Fuel Ratio Cntrl PL App (-0.15) | — FD Fan 1A Inlet Vlv Dmd PL App (-2.5)     | — FD Fan 1B Inlet Vlv Dmd PL App (-2.5)    | — FD Fan 1C Inlet Vlv Dmd PL App (2.5)      |
| — U1 AVG LF SECAIR BIAS (-1)             | — U1 AVG LF FDR BIAS (-1)                   | — U1 AVG LF PRIAIR BIAS (-1)               | — U1 AVG UF FDR BIAS (-1)                   |
| — U1 AVG UF PRIAIR BIAS (1)              | — U1 AVG UF SECAIR BIAS (1)                 | — U1 AVG LR FDR BIAS (1)                   | — U1 AVG LR PRIAIR BIAS (1)                 |
| — U1 AVG LR SECAIR BIAS (-1)             | — U1 AVG UR FDR BIAS (0.7148121)            | — U1 AVG UR PRIAIR BIAS (1)                | — U1 AVG UR SECAIR BIAS (1)                 |

# Impact on NH3 Usage



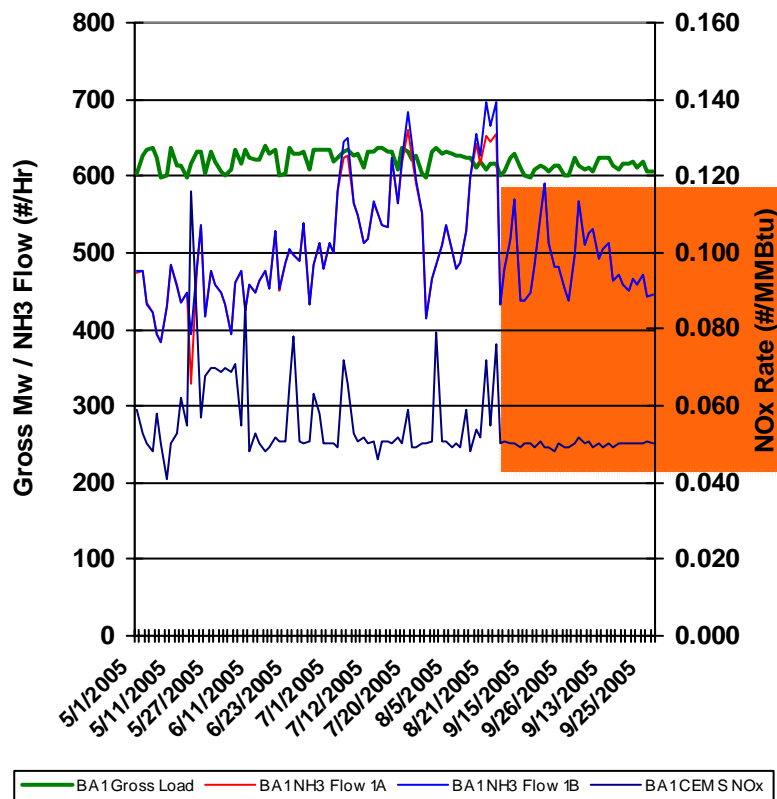
**WITHOUT Optimization, 400-600 klb/hr NH3 flow needed to meet NOx target**



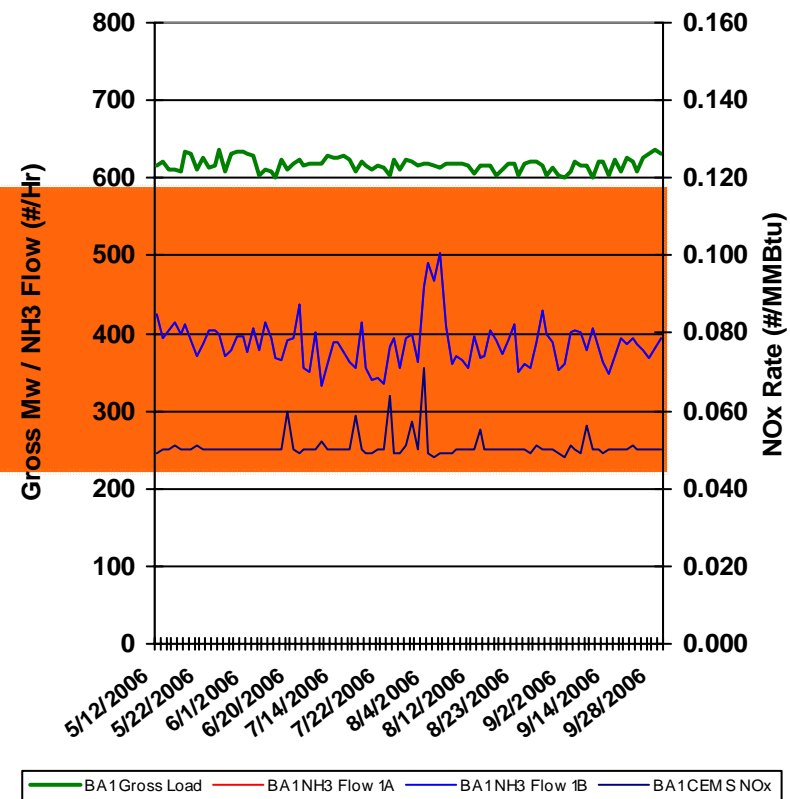
**WITH Optimization, 300-400 klb/hr NH3 flow needed to meet NOx target**

# Baldwin 1 – Full Load Comparison

Ozone Ammonia Flow - 2005



Ozone Ammonia Flow - 2006



# SootOpt

- **Context:**

- Sootblowing controls rely on interval-based or operator-initiated cleaning actions, or when using “intelligent” sootblowing systems, rely on zone cleanliness set points, ignoring the fact that optimal heat transfer requires varying cleanliness over time and across zones

- **What SootOpt Does:**

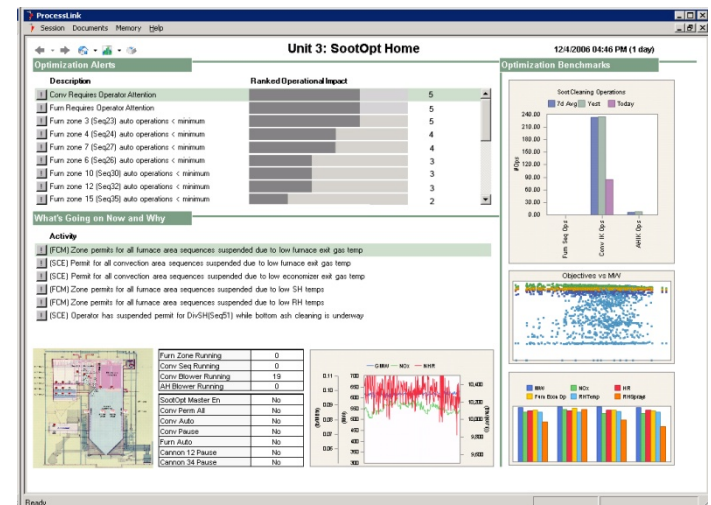
- Provides real-time closed-loop optimization of unit performance by manipulating all relevant sootblowing controls

- **Using:**

- Expert systems, neural networks and model predictive control

- **To Achieve:**

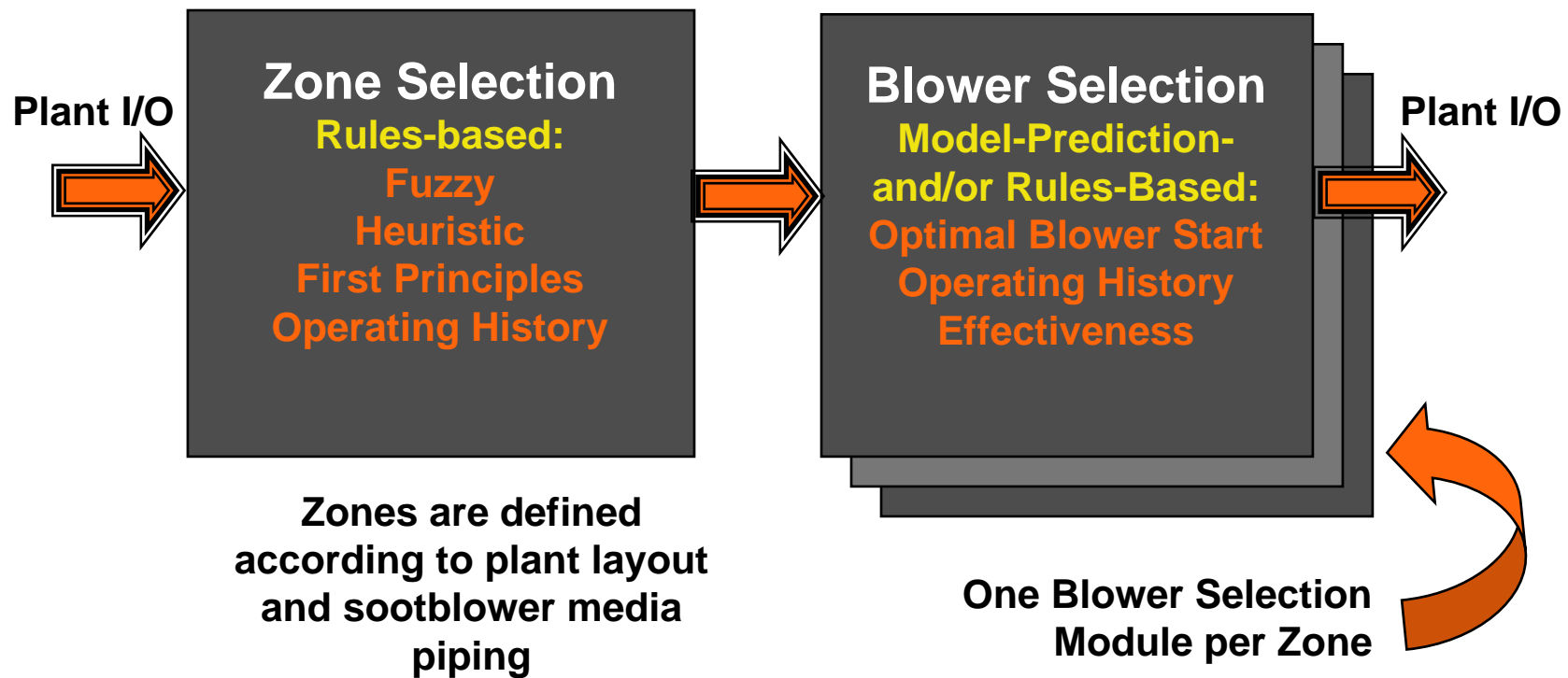
- Reliability, heat rate, steam temp and emissions improvements



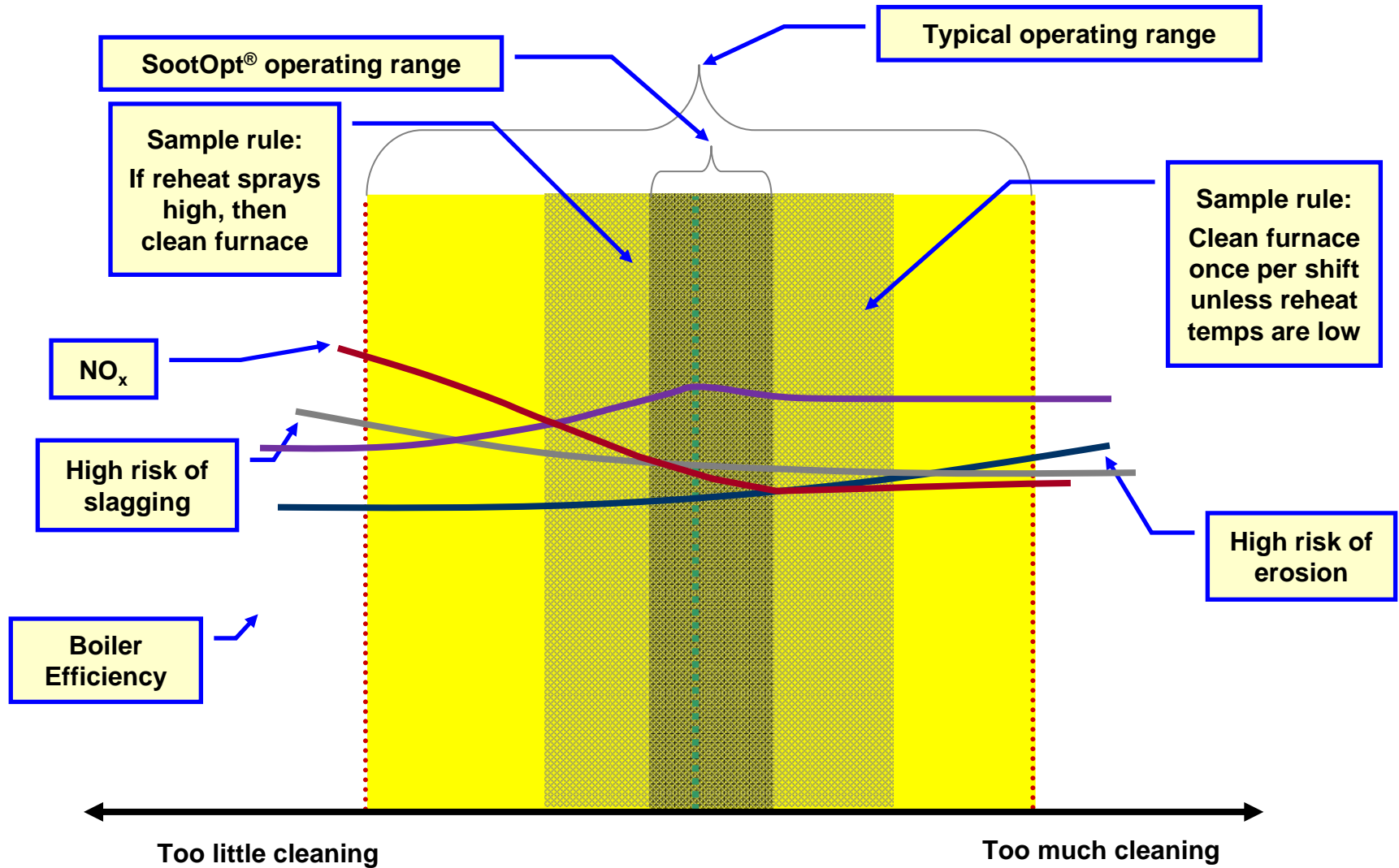
# Overview: What SootOpt does

- Improves heat rate
  - by improving heat transfer and heat transfer distribution
  - Be improving steam temperature control
  - by reducing use of attemperation spray and sootblowing media (steam, water, air)
- Improves availability
  - Reduced blowing reduces tube erosion and thermal fatigue
- Improves NOx control
  - through improved heat transfer, reduction of “hot spots”, and reduced firing intensity
- Reduces opacity violations
  - by using opacity data in decision-making
- Reduces operator workload and improves shift-to-shift consistency

# Overview: How SootOpt Works



# Sootblower Optimization



ProcessLink  
 Session Documents Debug Help

### Unit 3: SootOpt Home

8/22/2008 11:23 AM (1 day)

#### Optimization Alerts

Issue/Action	Actual	Target	!!!
Some SH boiler IKs 1A, 1, 2 are below minimum required ops	1	0	!!!
Some RH boiler IKs 11-14 are over expected ops	1	0	!!!

**SootOpt® Summary Line**      **Optimization Alerts**

#### Optimization Analysis

Last Evaluation: 8/22/2008 11:22:07 AM, Goal: Reduce APH 3A Gas In Temp, Zone: SH\_Economizer, Device: SH12\_72      Blower Select: Model

##### Zone Selection:

Goal	Zone	Eligible	Applica...
Lower RH Steam Temp	RH_Platen	✗	✓
Lower RH Steam Temp	RH_Furnace	✗	✓
Reduce APH 3A Gas In Temp	SH_Convection	✗	✓
Reduce APH 3A Gas In Temp	SH_Economizer	✓	✓
Reduce APH 3A Gas In Temp	SH_Platen	✓	✓
Reduce APH 3A Gas In Temp	SH_Furnace	✗	✓
Reduce APH 3B Gas In Temp	RH_Furnace	✗	✓
Reduce APH 3B Gas In Temp	RH_Platen	✗	✓

**Rule Selection Table**

##### Blower Selection:

Blower	Eligible	Idle	Rank
SH11_71	✓	●	
SH12_72	✗	●	
SH13_73	✗	●	
SH14_74	✓	●	

**Blower Selection Table**

#### Optimization Benchmarks

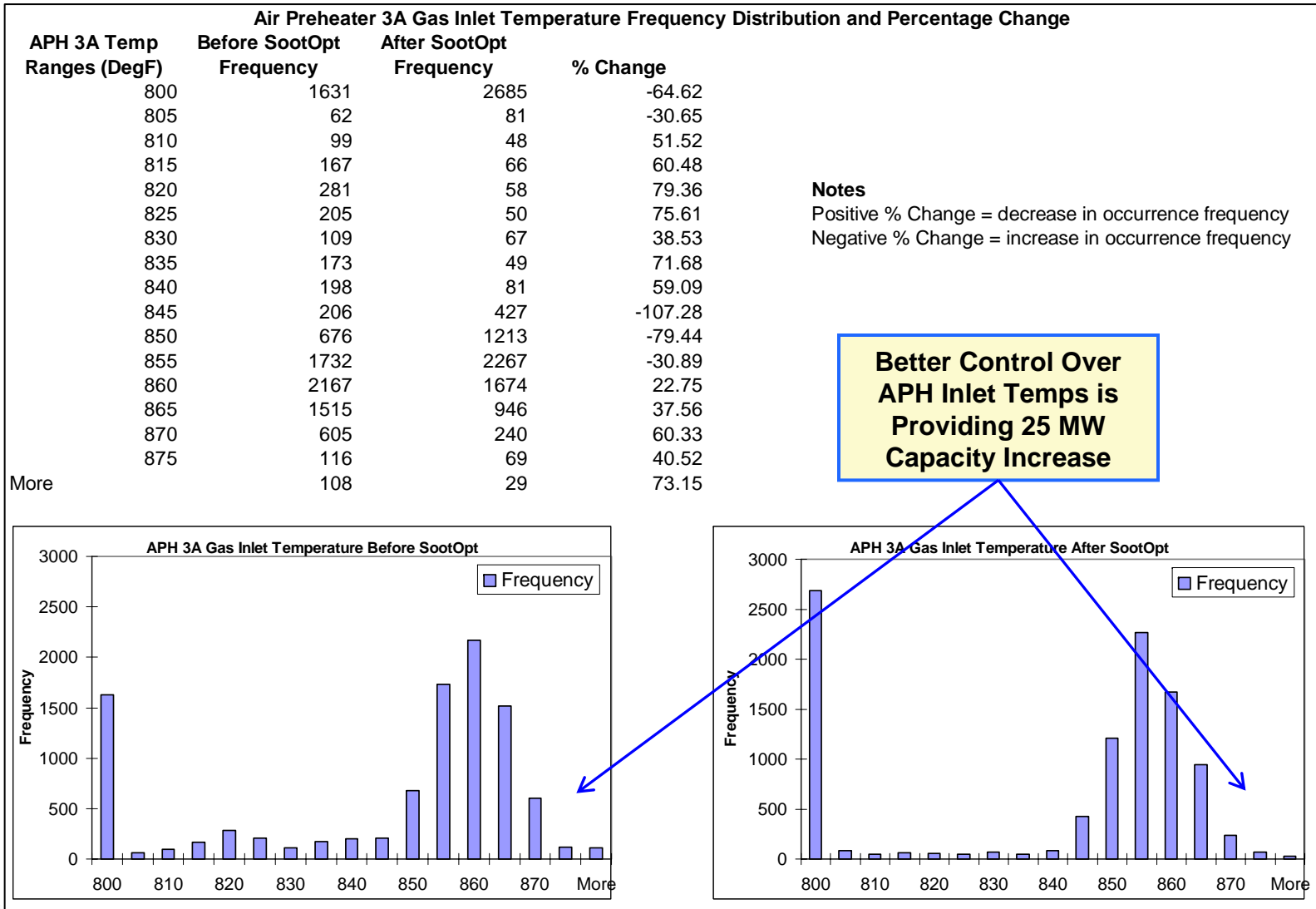
Average Steam Temperatures, SootOpt On vs. Off

Average Gas Temperatures, SootOpt On vs. Off

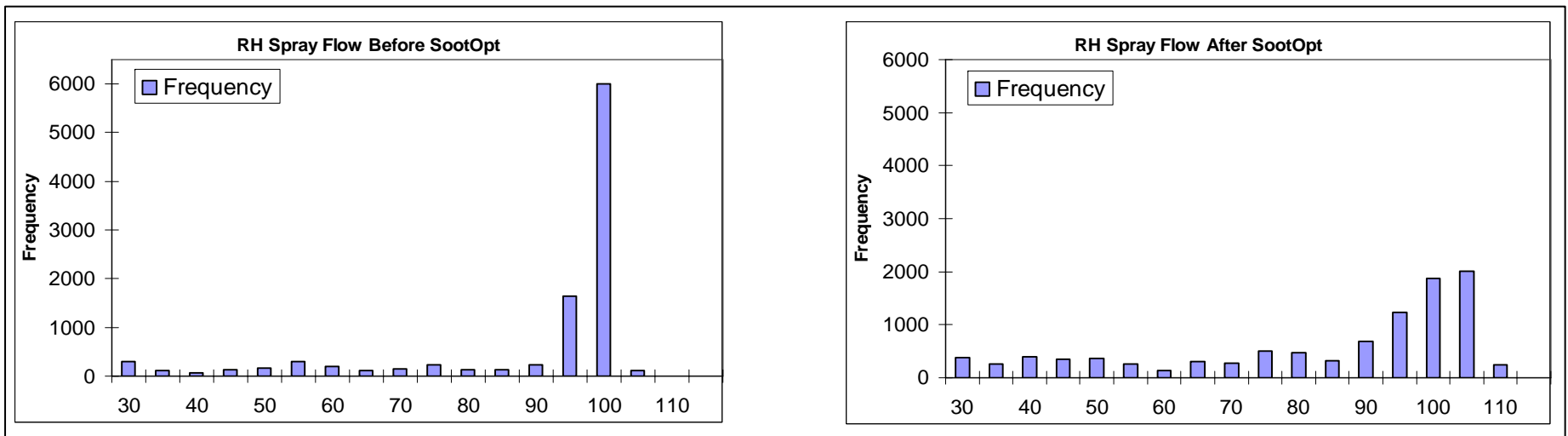
Average Unit Load, Heat Rate and NOx, SootOpt On vs. Off

Loading page...

# Meramec APH Temps - SootOpt ON-OFF Comparison



# Meramec RH Sprays - SootOpt ON-OFF Comparison



# Summary of Meramec SootOpt Benefits

- Narrowed superheat and reheat steam temperature variability and moved closer to setpoint
- Simultaneously reduced attemperation sprays
- Reduced manually blowing of three lances in less than half
- No erosion-related tube leaks in at least *seven months*, relative to history of every 2-8 weeks
- Improved the operators' effectiveness:
  - Before, operators had to manually manage sootblowing
  - Now they operators spend very little time managing sootblowing.
  - “We just put in SootOpt and let it fly.”